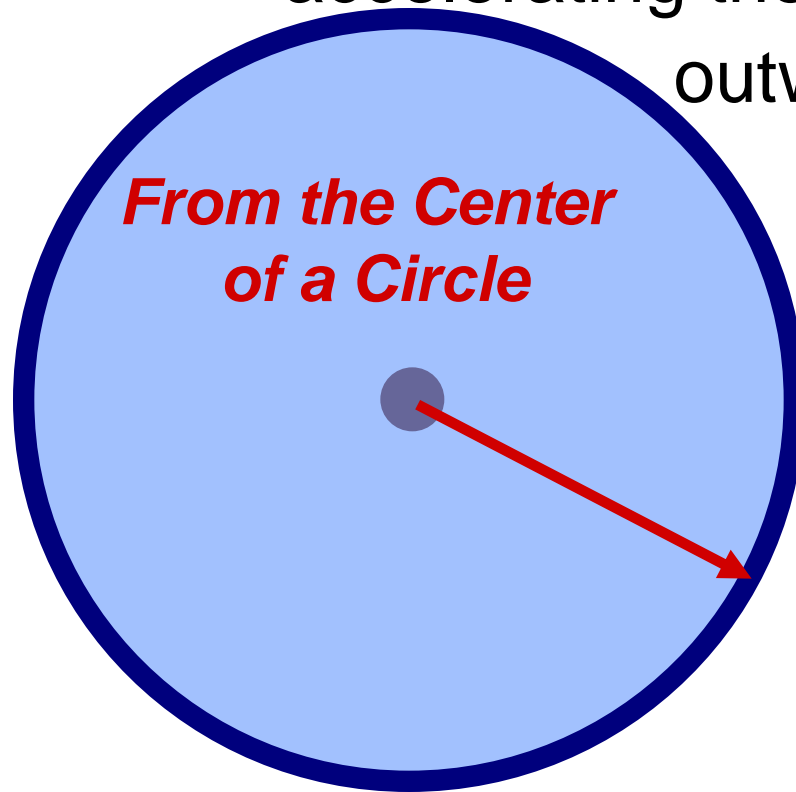




Centrifugal Pumps

A machine for moving fluid by accelerating the fluid *RADIALLY* outward.

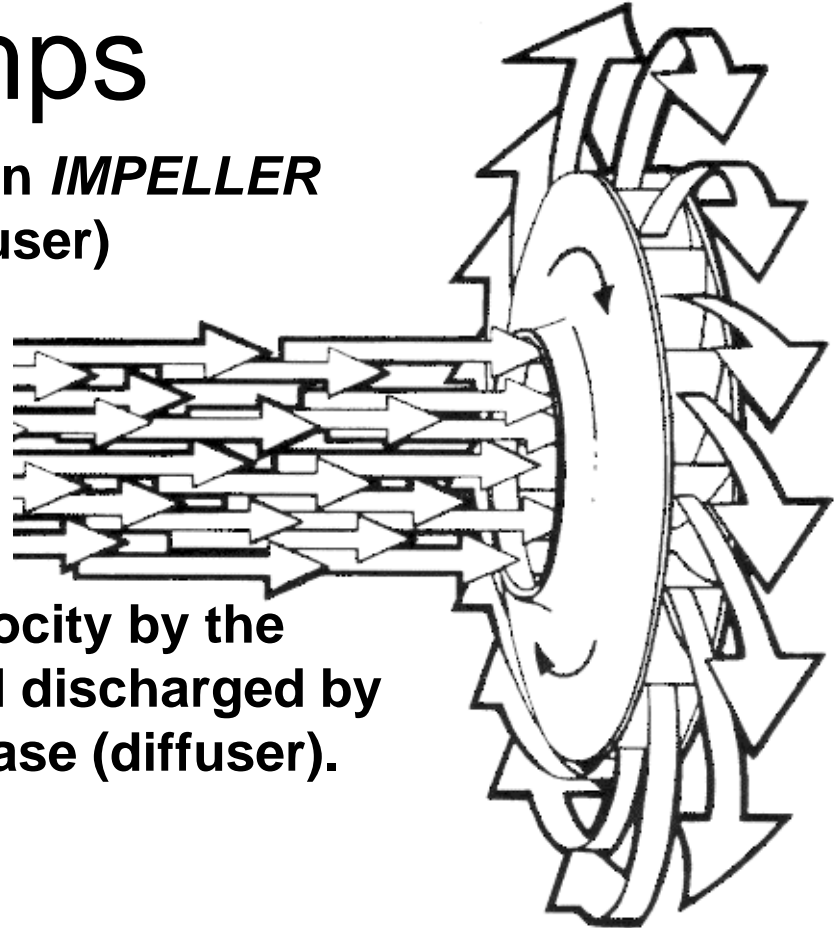


***From the Center
of a Circle***

***RADIAL DIRECTION
To the Outside of a Circle***

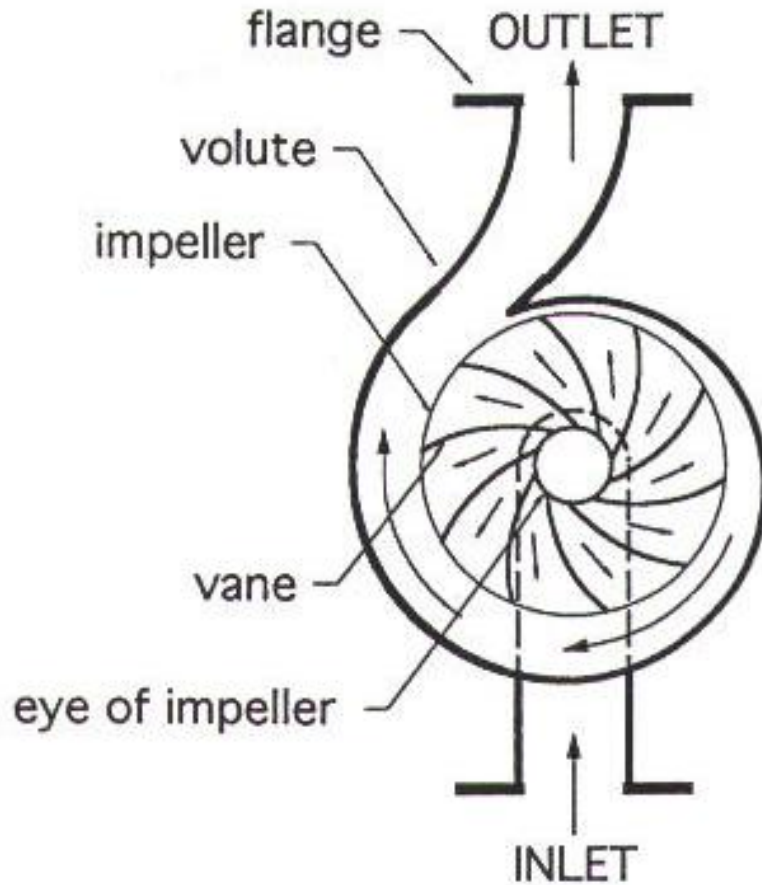
Centrifugal Pumps

- This machine consists of an *IMPELLER* rotating within a case (diffuser)
- Liquid directed into the center of the rotating impeller is picked up by the impeller's vanes and accelerated to a higher velocity by the rotation of the impeller and discharged by centrifugal force into the case (diffuser).



Centrifugal Pumps

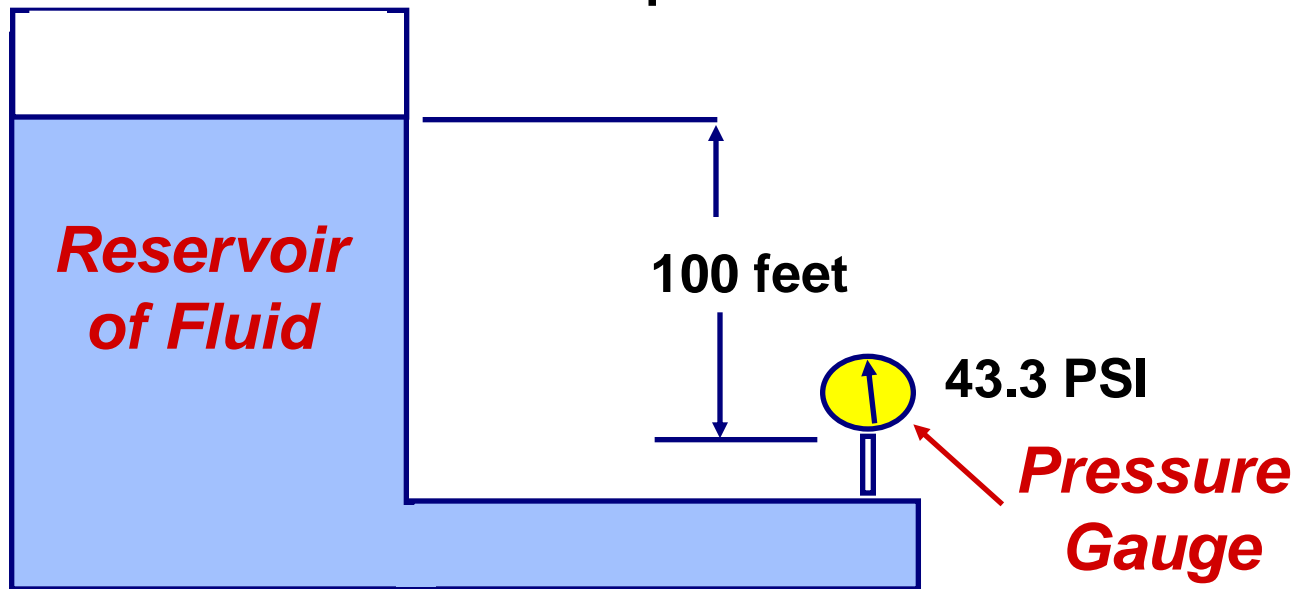
- A collection chamber in the casing converts much of the **Kinetic Energy** (energy due to velocity) into ***Head or Pressure***.



Pump Terminology

"Head"

- Head is a term for expressing feet of water column
- Head can also be converted to pressure



Conversion Factors Between Head and Pressure

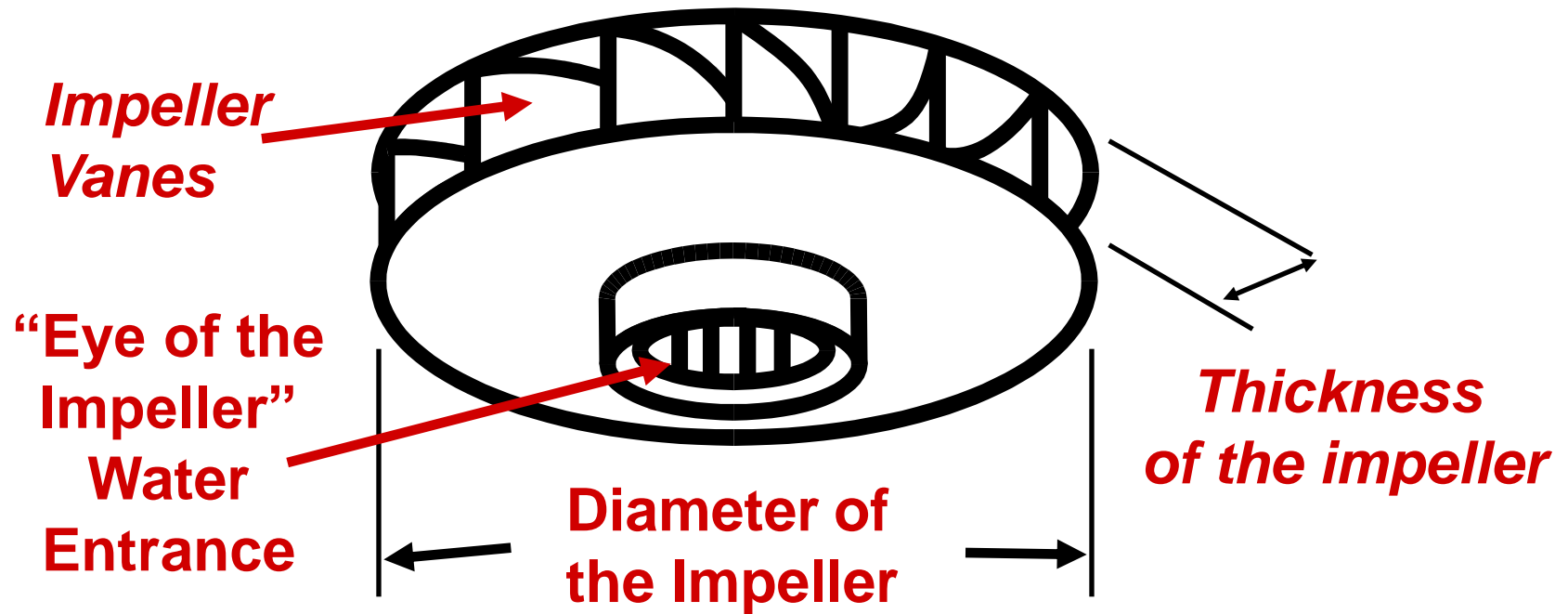
- **Head (feet of liquid) = Pressure in PSI x 2.31 / Sp. Gr.**
- **Pressure in PSI = Head (in feet) x Sp. Gr. / 2.31**
- **PSI is Pounds per Square Inch**
- **Sp. Gr. is Specific Gravity which for water is equal to 1**
 - **For a fluid more dense than water, Sp. Gr. is greater than 1**
 - **For a fluid less dense than water, Sp. Gr. is less than 1**



Head

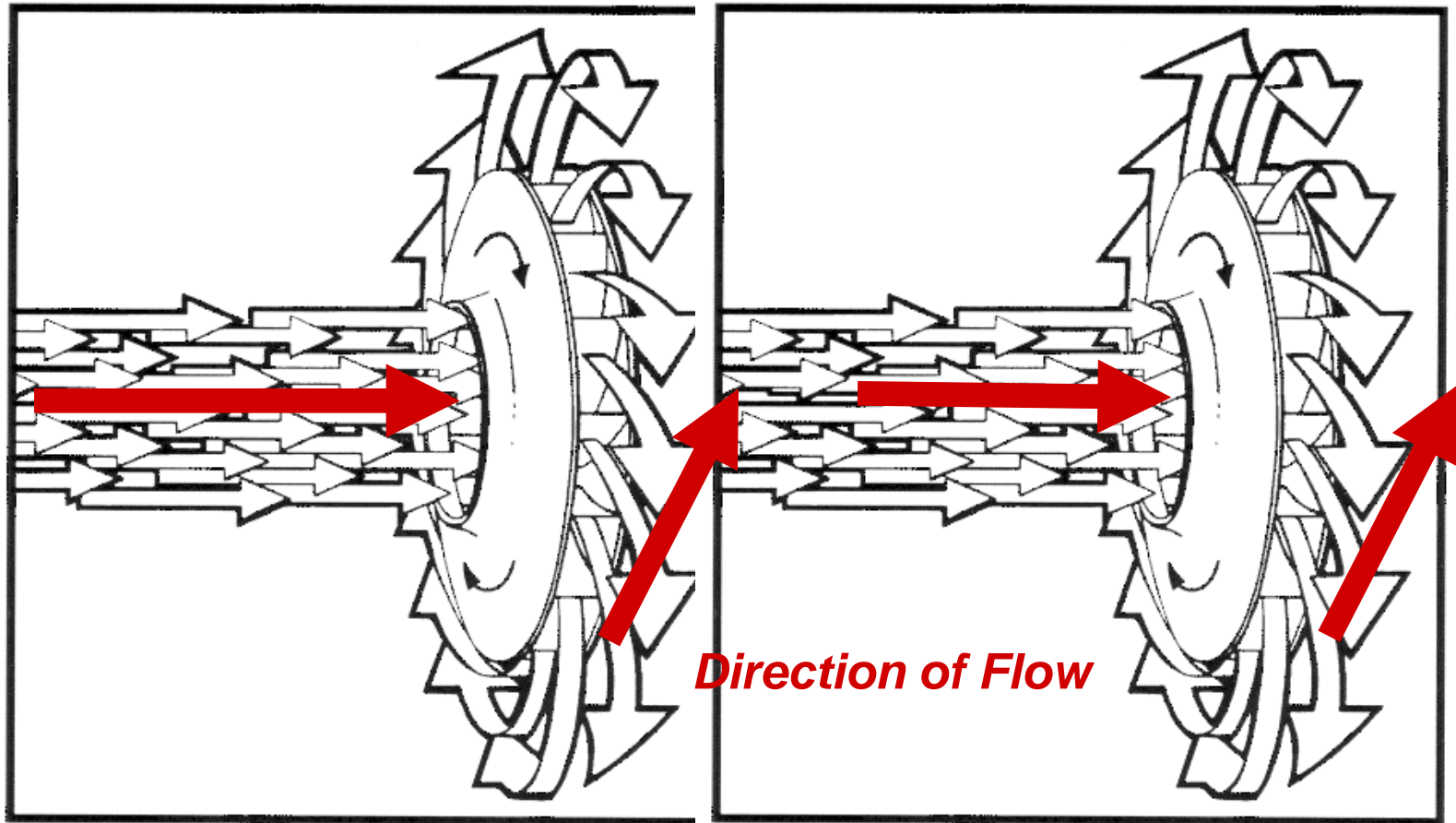
- Head and pressure are interchangeable terms provided that they are expressed in their correct units.
- The conversion of all pressure terms into units of equivalent head simplifies most pump calculations.

Centrifugal Impellers



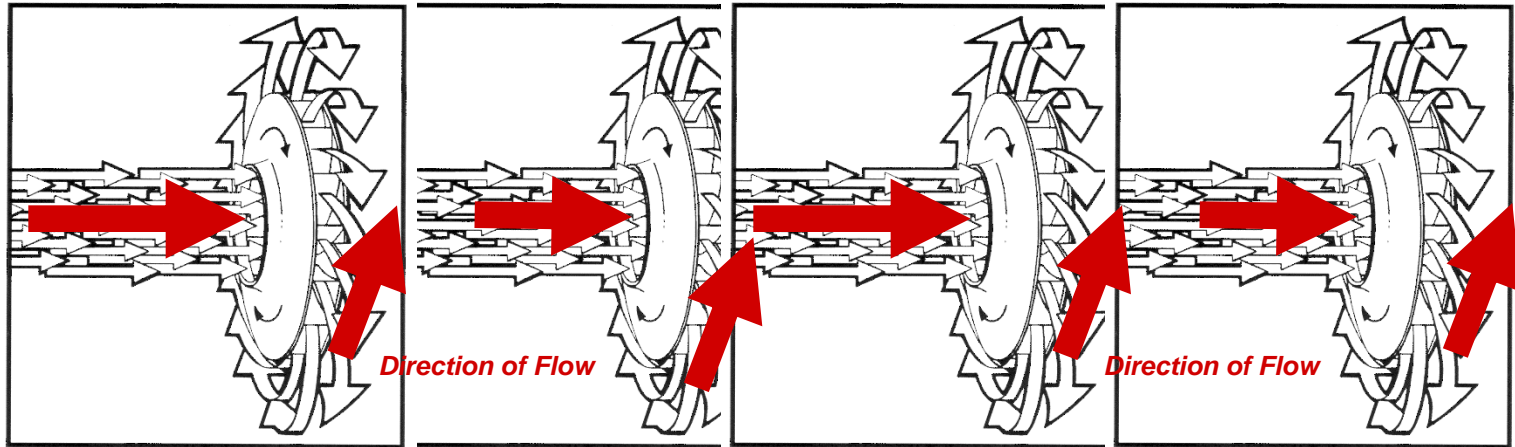
- Thicker the Impeller- More Water
- Larger the DIAMETER - More Pressure
- Increase the Speed - More Water and Pressure

Two Impellers in Series



- Twice the pressure
- Same amount of water

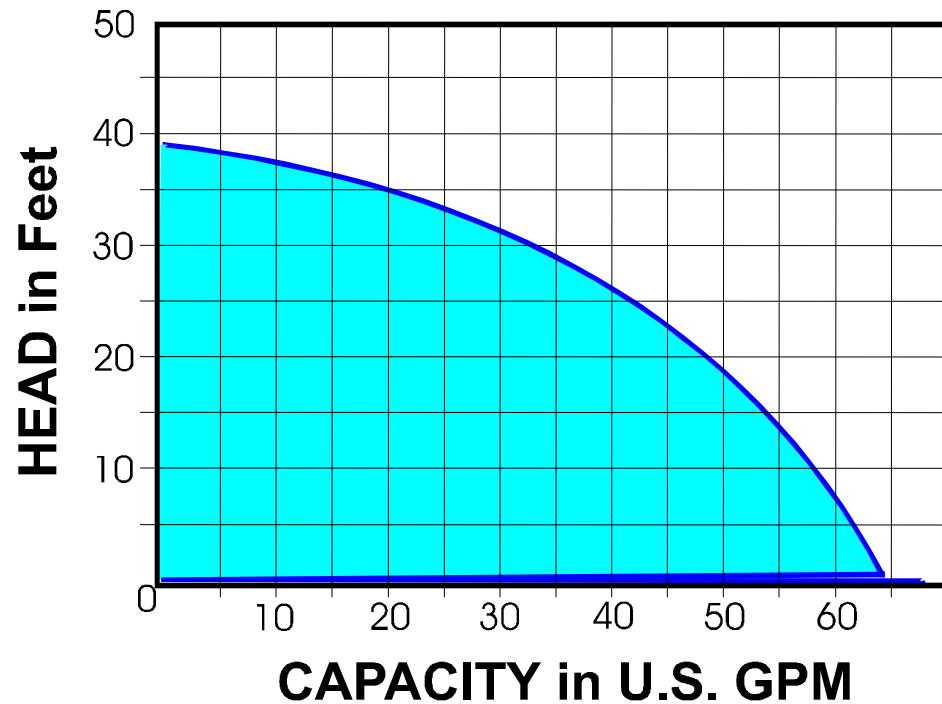
Multiple Impellers in Series



- Placing impellers in series increases the amount of head produced
- The head produced = # of impellers x head of one impeller

Pump Performance Curve

- A mapping or graphing of the pump's ability to produce head and flow



Pump Performance Curve

Step #1, Horizontal Axis

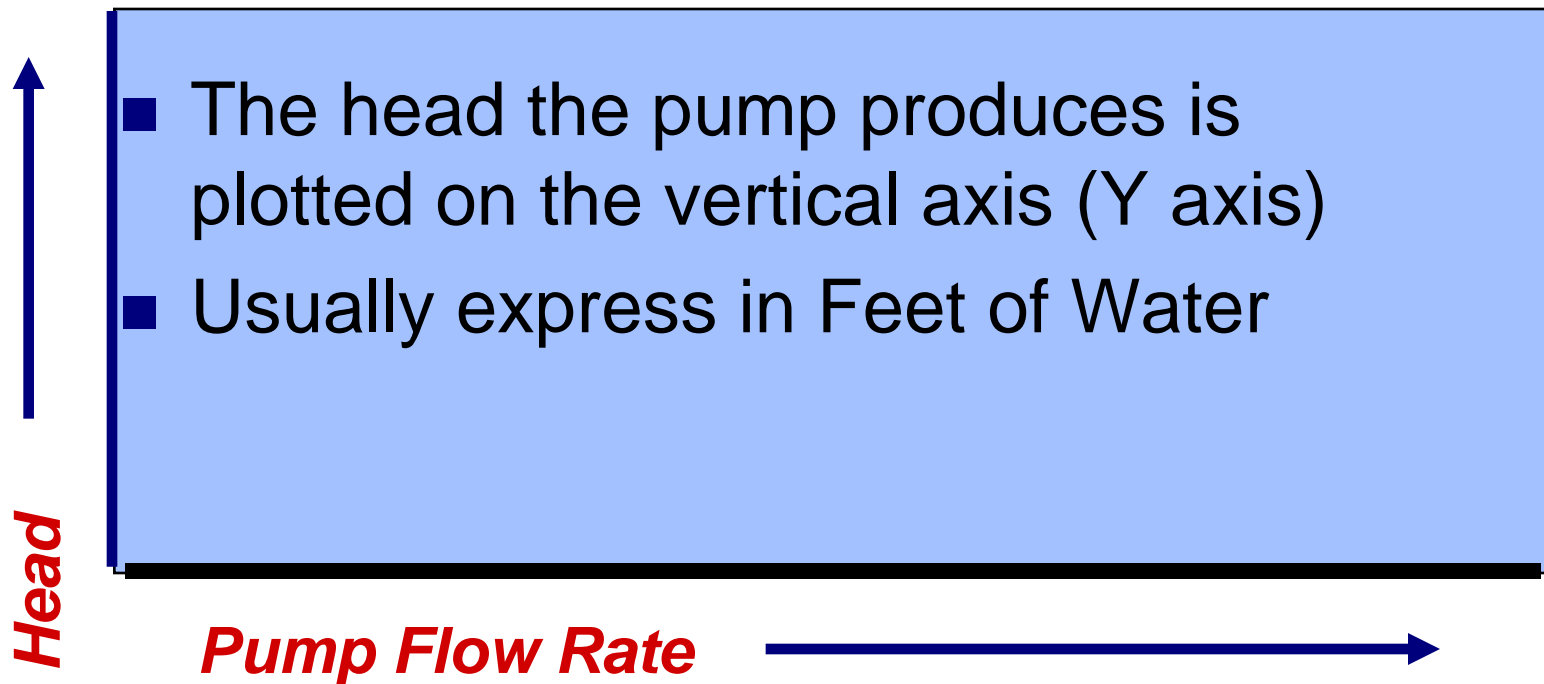
- The pump's flow rate is plotted on the horizontal axis (X axis)
- Usually expressed in Gallons per Minute

Pump Flow Rate



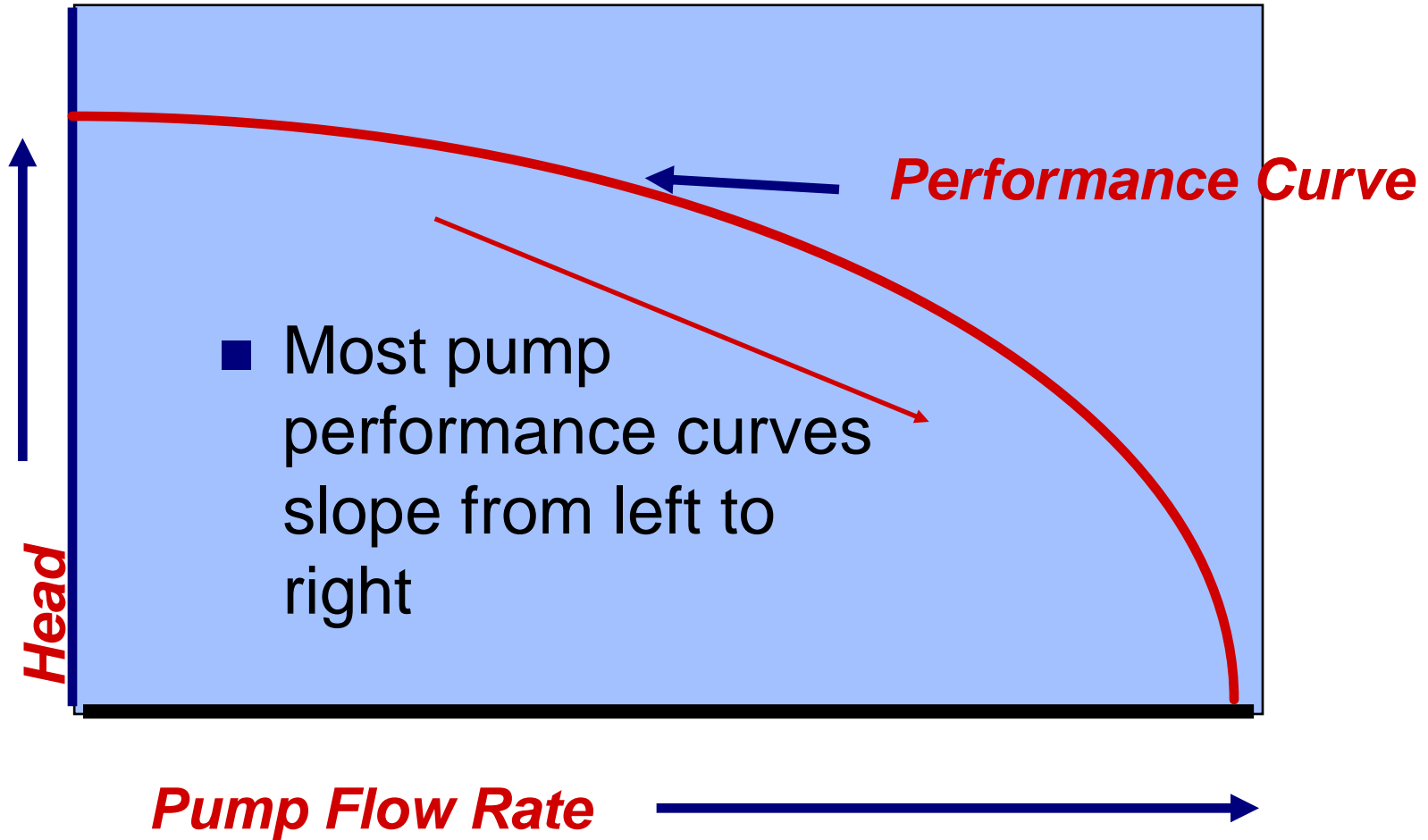
Pump Performance Curve

Step #2, Vertical Axis



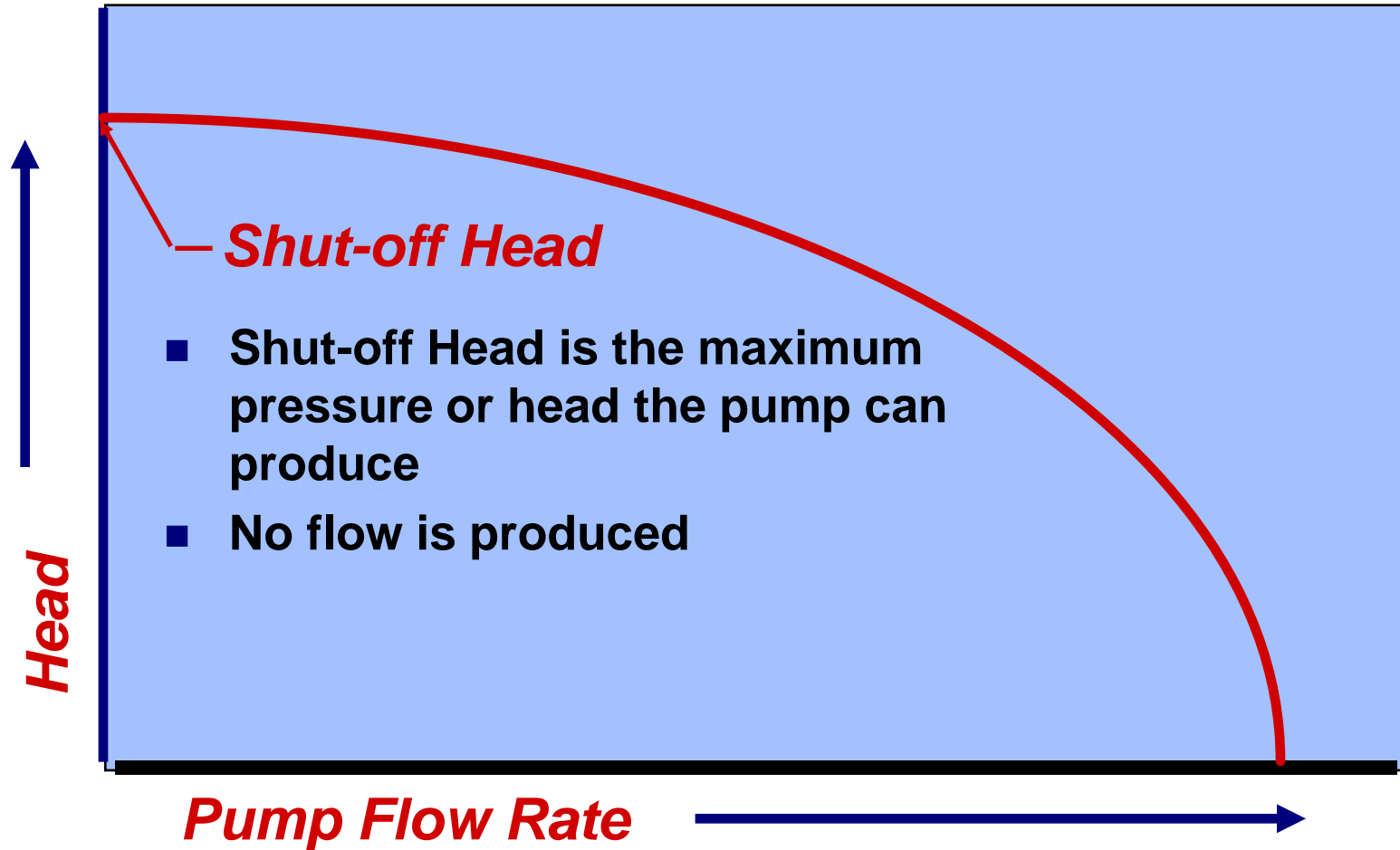
Pump Performance Curve

Step #3, Mapping the Flow and the Head



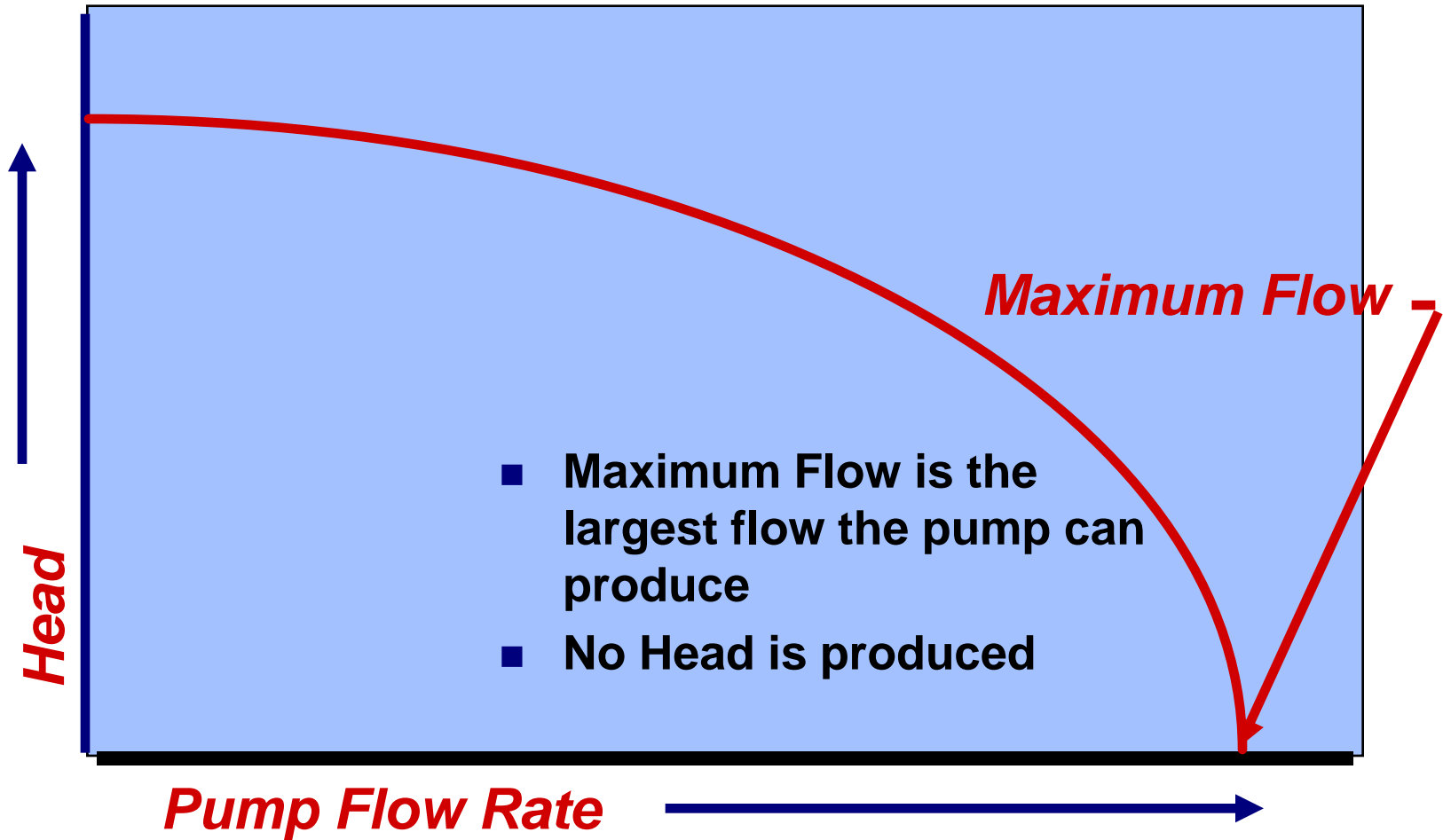
Pump Performance Curve

Important Points



Pump Performance Curve

Important Points



System Performance Curves

- System Performance Curve is a mapping of the head required to produce flow in a given system
- A system includes all the pipe, fittings and devices the fluid must flow through, and represents the friction loss the fluid experiences

System Performance Curve

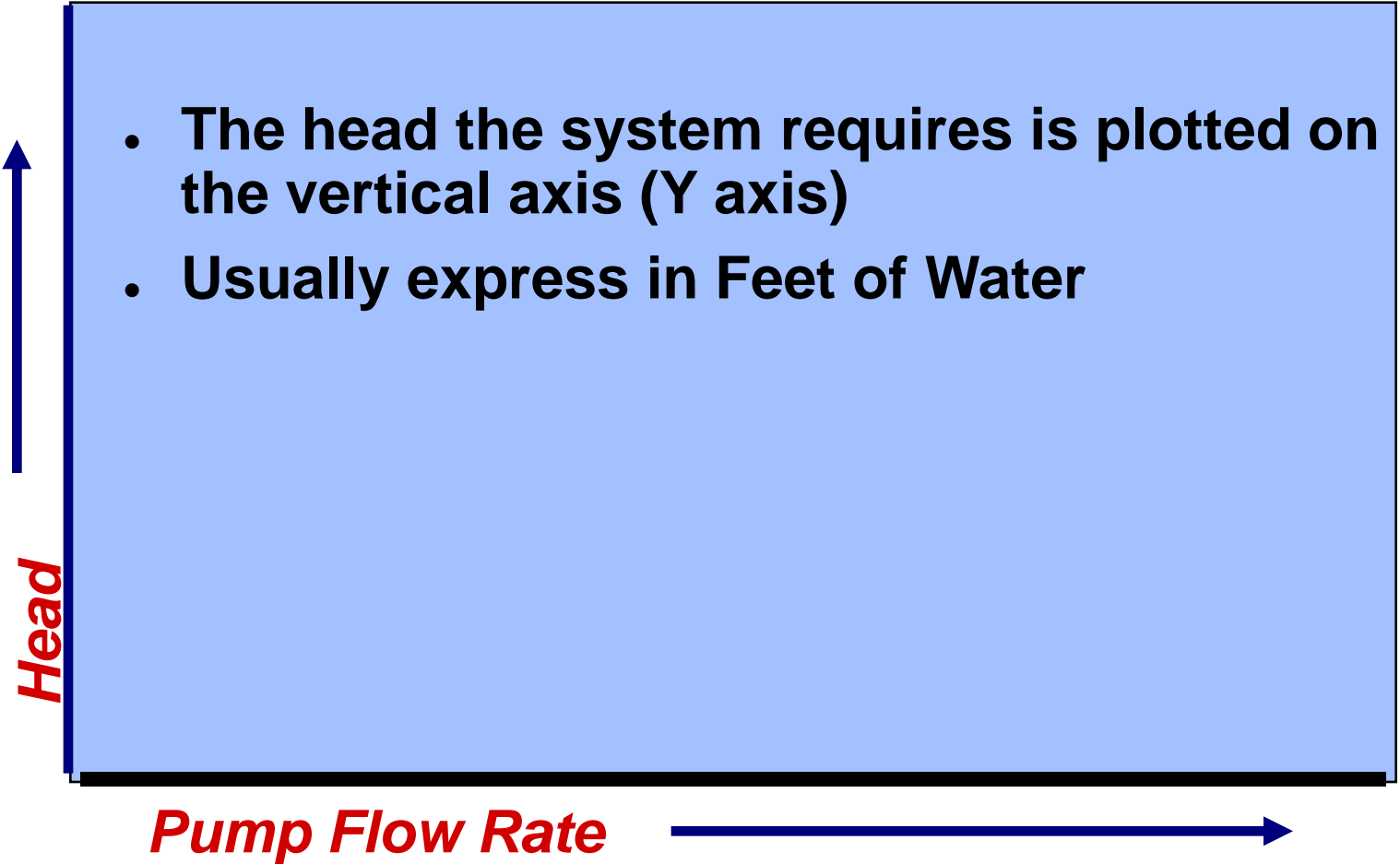
Step #1, Horizontal Axis

- The System's flow rate is plotted on the horizontal axis (X axis)
- Usually expressed in Gallons per Minute

System Flow Rate 

System Performance Curve

Step #2, Vertical Axis

- 
- The head the system requires is plotted on the vertical axis (Y axis)
 - Usually express in Feet of Water

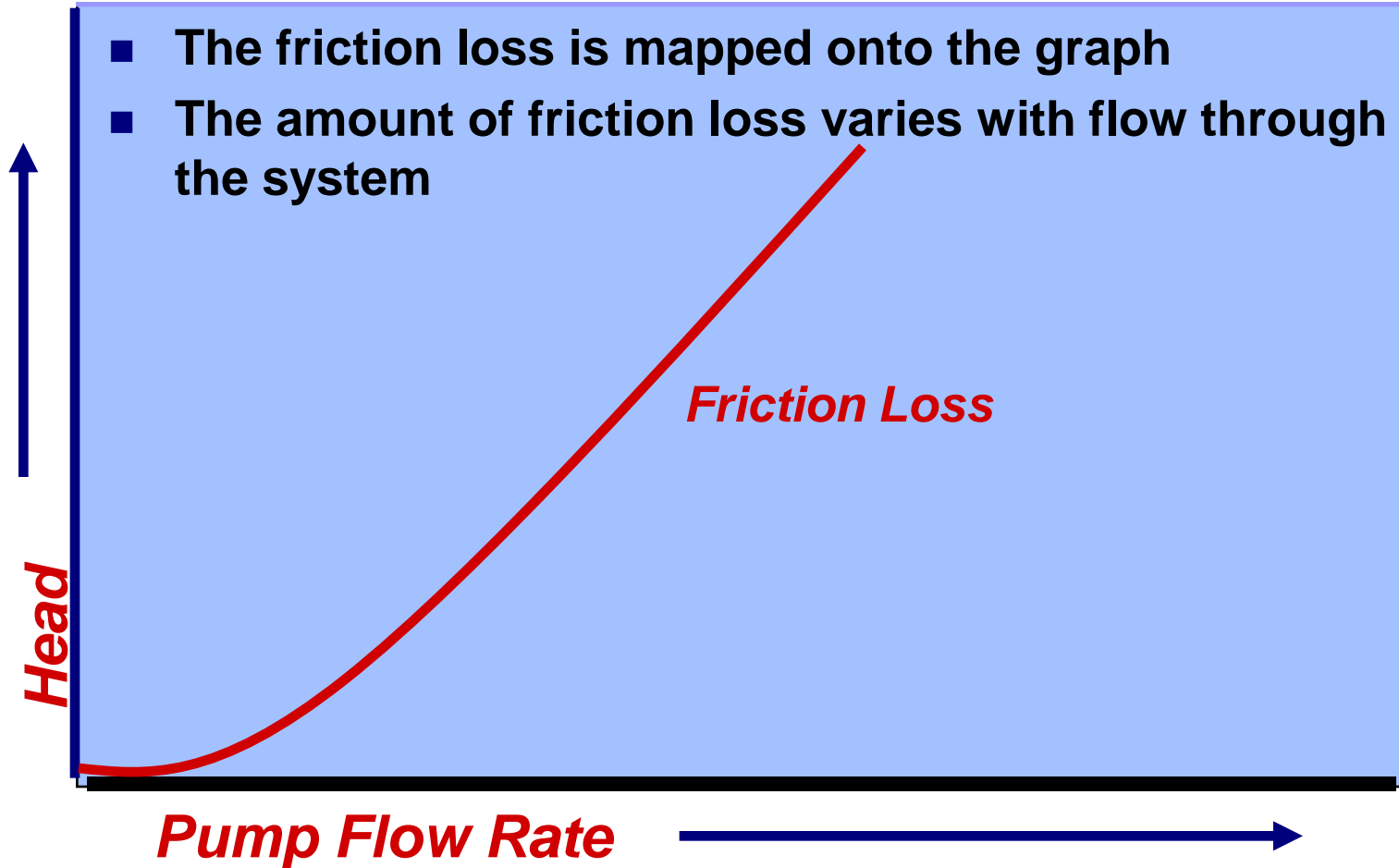
Head

Pump Flow Rate

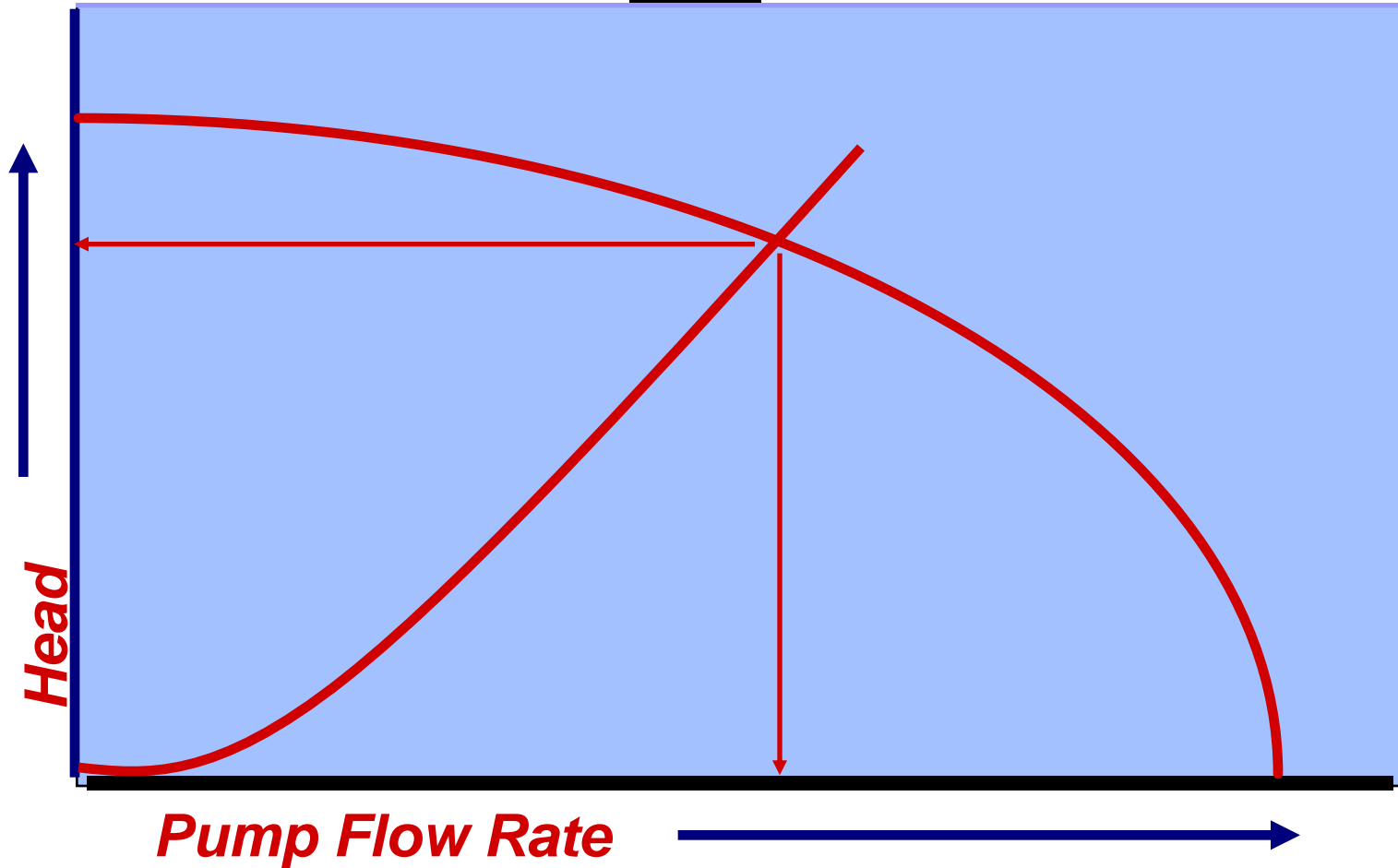
System Performance Curve

Step #3, Curve Mapping

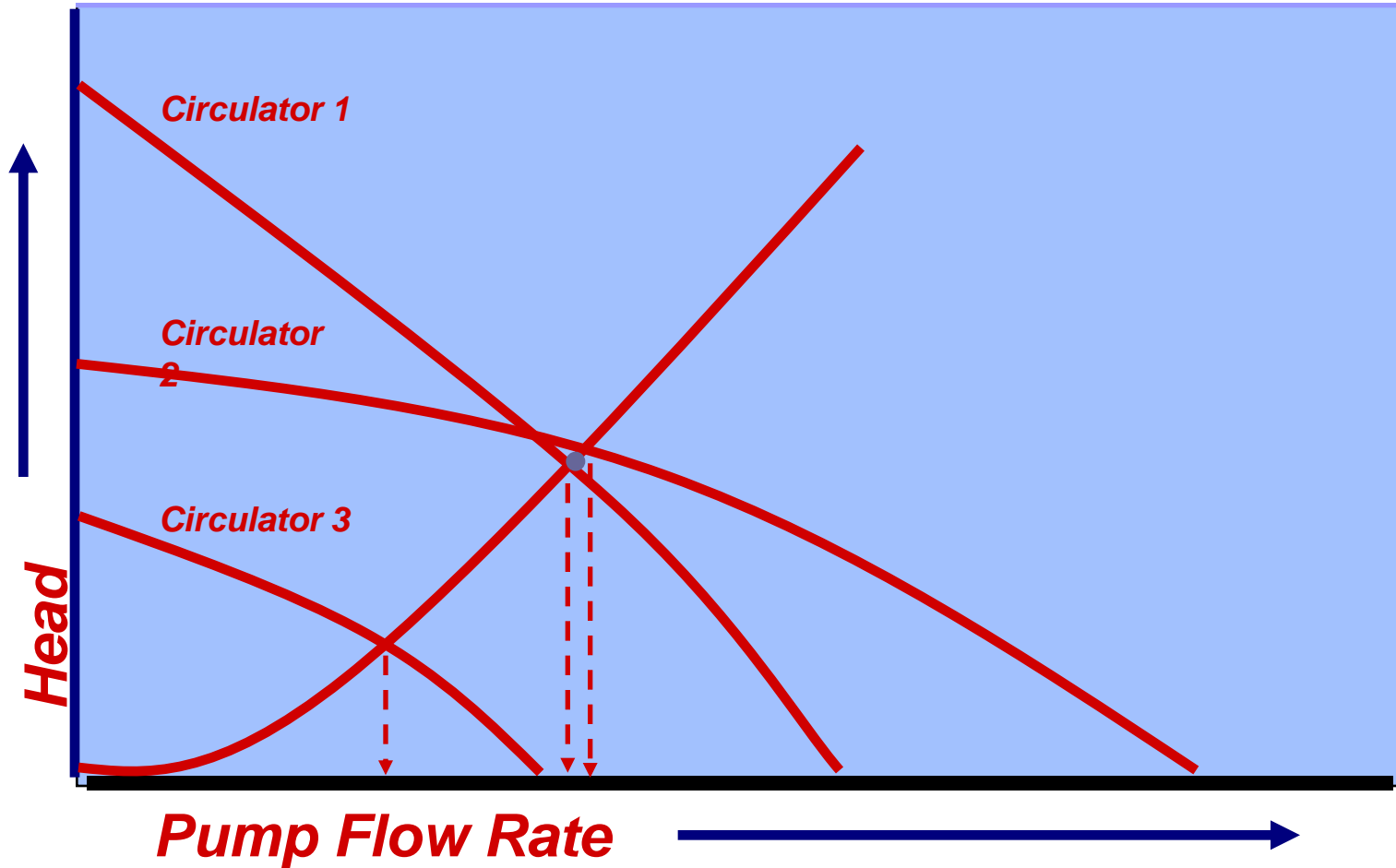
- The friction loss is mapped onto the graph
- The amount of friction loss varies with flow through the system



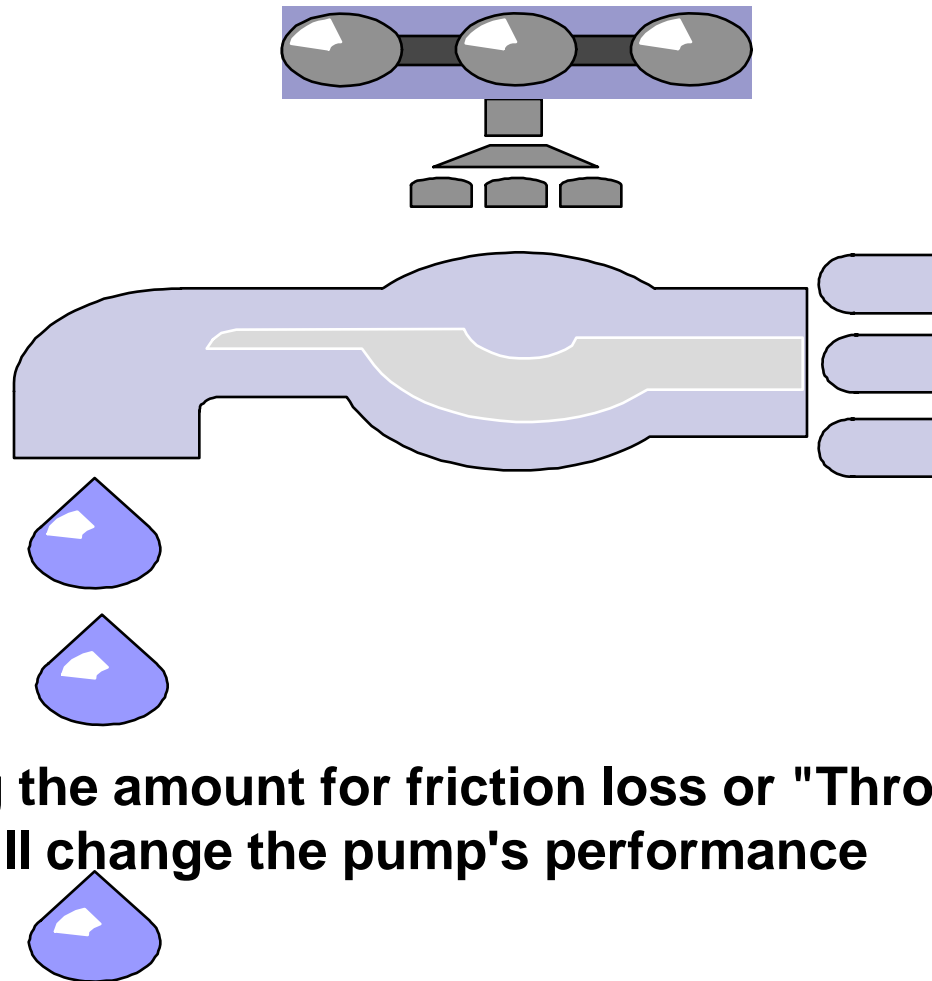
The point on the system curve that intersects the pump curve is known as the operating point.



PUMP SELECTION

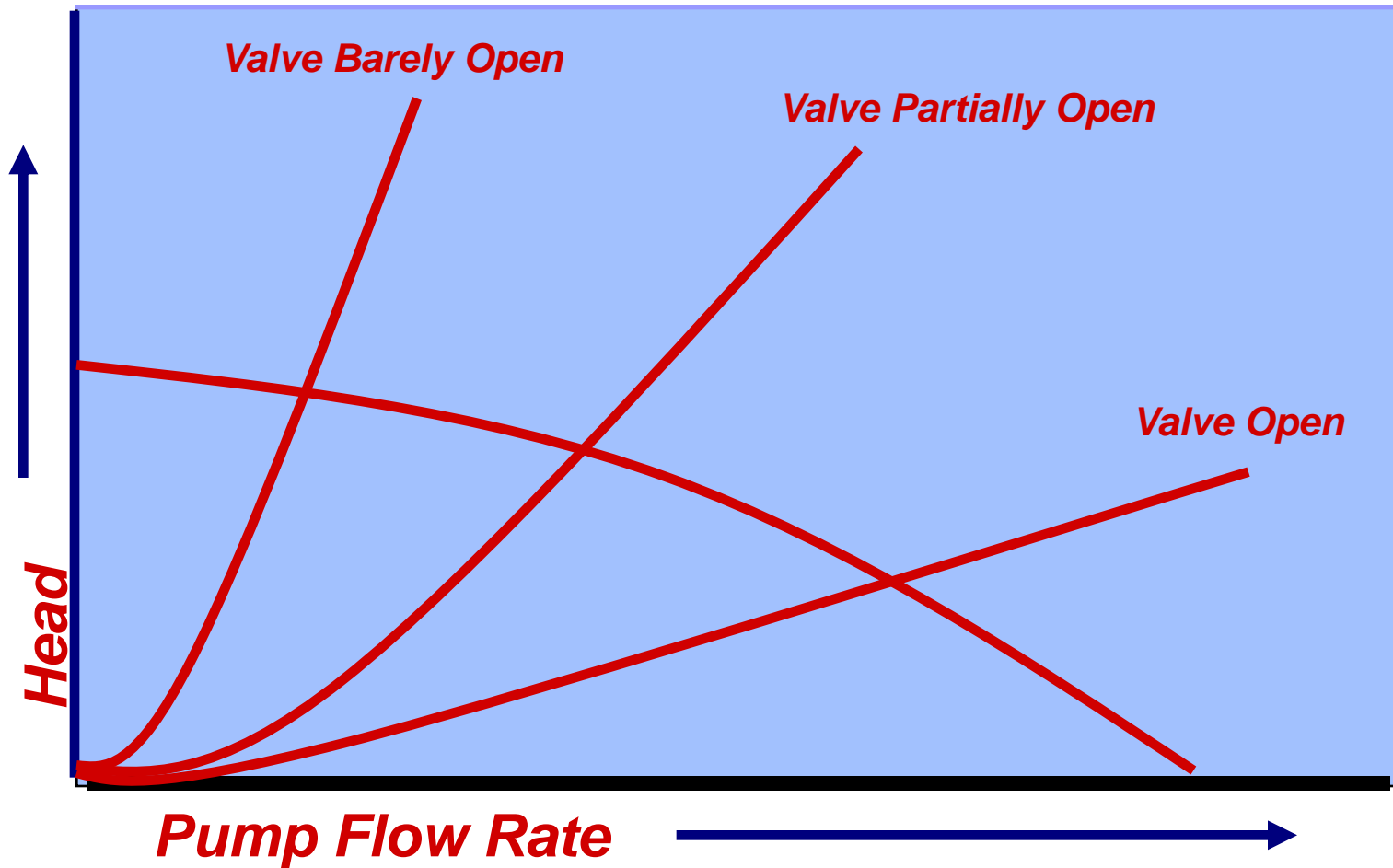


Controlling Pump Performance




- Changing the amount for friction loss or "Throttling the Pump" will change the pump's performance

PUMP SELECTION



File Actions Settings Help



Proposal Header

Selection

Items

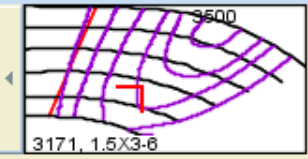
Previous

Continue

Criteria Results Curves

Create PDF

Modify



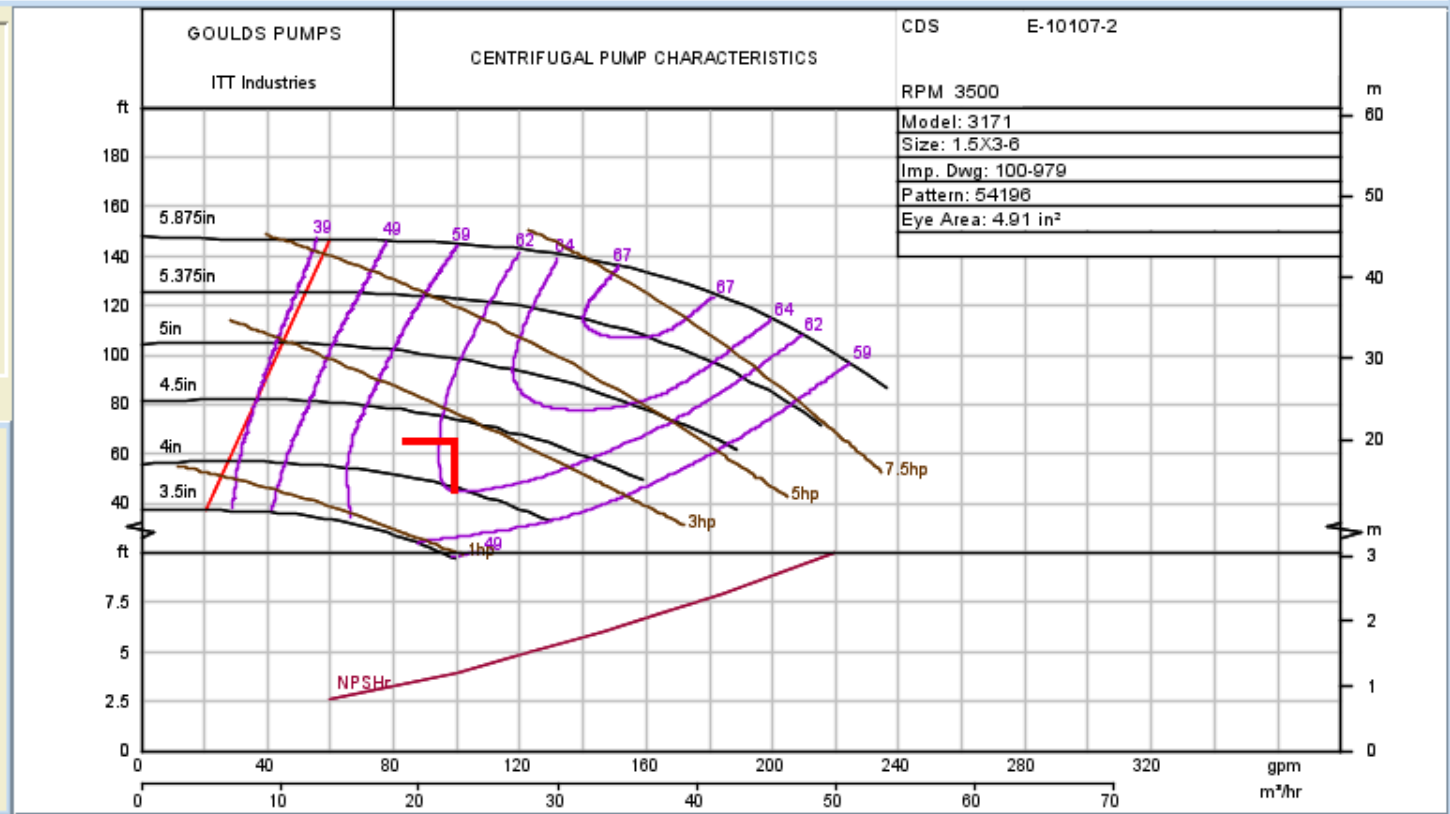
Cds Line

Design

Speed	3500
Diam.	4.3750 in
Flow	100.0 gpm
Head	66.3 ft
NPSHr	4.0 ft
Eff.	64.0
Power	2.6 hp
Sp. Gr.	1.000
Visc.	1.000 cp

View View Add.

- Head vs. Flow
- Power
- Efficiency
- NPSH
- Design Point
- Add'l Des. Points
- System Curves



Piping Design Equations

Heuristics for Pipe Diameter

Liquids :

$$D = 2.607 \left(\frac{w}{\rho} \right)^{0.494}$$

Gases :

$$D = 1.065 \left(\frac{w^{0.408}}{\rho^{0.343}} \right)$$

D = Diameter, inches

w = Mass Flowrate, 1000 lb / hr

ρ = Density, lb / ft³

Energy Loss in Piping Networks

Incompressible Fluids

$$\frac{144}{\rho}(P_1 - P_2) + \frac{1}{2g}(v_1^2 - v_2^2) = (z_2 - z_1) + h_L$$

$\rho = \text{Density, } lb / ft^3$


$P = \text{Pressure, } lb_f / in^2$

$v = \text{Velocity, } ft / sec$

$g = \text{Gravitational Acceleration, } 32.174 ft / s^2$

$z = \text{Elevation, } ft$

$h_L = \text{Head loss, } ft$


$$h_L = \frac{0.00259 \left(\sum K \right) Q^2}{d^4}$$

$Q =$ *Volumetric Flowrate, gpm*

$d =$ *Pipe Diameter, in*

$\sum K =$ *Sum of all fittings*

$K = f \frac{L}{D}$, *straight pipe*

$K = \left(1 - \frac{d_1^2}{d_2^2} \right)^2$, *Sudden enlargement*

Friction Loss Factors for Fittings

Fitting	K
Standard 90° Elbow	$30f_T$
Standard 45° Elbow	$16f_T$
Standard Tee	$20f_T$ Run $60 f_T$ Branch
Pipe Entrance	0.78
Pipe Exit	1.0

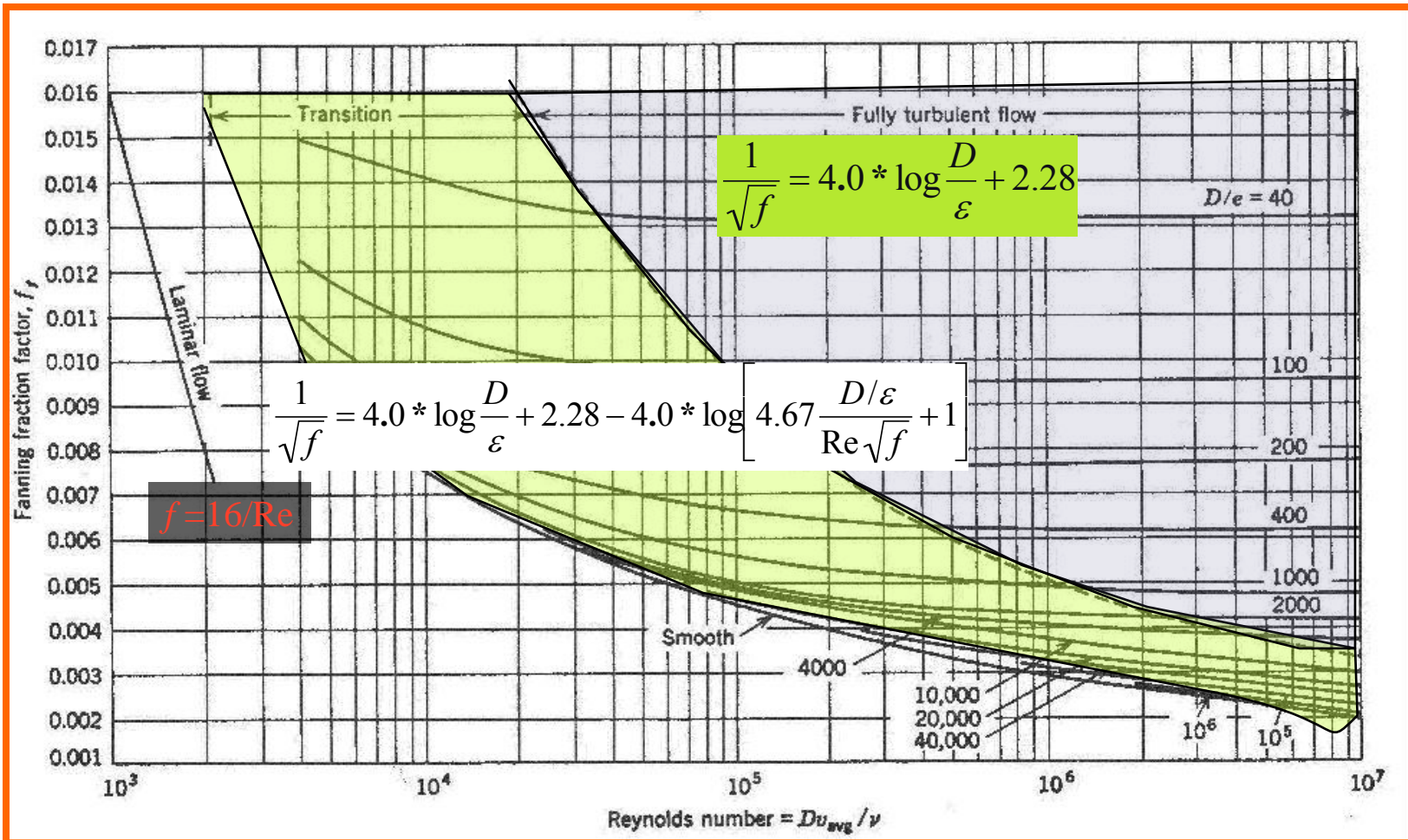
Friction Loss Factors for Valves

Valve	K
Gate valve	$8f_T$
Globe Valve	$340f_T$
Swing Check Valve	$100f_T$
Lift Check Valve	$600f_T$
Ball Valve	$3f_T$

$$\sqrt{K} = \frac{29.9d^2}{C_V^2}$$

$C_V = \text{Valve Coefficient}$

Fanning Diagram



Energy Loss in Valves

- Function of valve type and valve position
- The complex flow path through valves can result in high head loss (of course, one of the purposes of a valve is to create head loss when it is not fully open)
- E_v are the loss in terms of velocity heads

